

Original article

# Molecular dynamics study of H<sub>2</sub>-oil mixture behavior in shale nanopores

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**Abstract:**

With growing hydrogen demand and production, large-scale H<sub>2</sub> storage technologies are becoming increasingly essential. Depleted shale reservoirs, with their extensive pore space and existing subsurface infrastructure, offer a promising option for large-scale H<sub>2</sub> storage. In this study, the behavior of H<sub>2</sub> in shale nanopores in the presence of residual oil, which has not been well explored, is systematically investigated. It is observed that at 353 K and 30 MPa, residual oil weakens but does not completely prevent H<sub>2</sub> accumulation on pore surfaces, which may contribute to H<sub>2</sub> loss. Furthermore, decreasing pore size enhances H<sub>2</sub> surface accumulation due to nano-confinement effect, while increased oil saturation and smaller apertures reduce H<sub>2</sub> self-diffusion by restricting transport pathways. In addition, the phase of oil also plays a key role: supercritical methane mixes readily with H<sub>2</sub>, whereas liquid n-butane, n-octane, and n-dodecane form clusters or oil bridges, further limiting H<sub>2</sub> mobility in nanopores. These findings provide molecular-scale insights into H<sub>2</sub>-oil interactions and highlight the combined effects of residual oil saturation, pore size, and oil composition on H<sub>2</sub> retention and transport, which are critical for assessing the feasibility of underground H<sub>2</sub> storage in depleted shale reservoirs.

## 1. Introduction

Hydrogen, known for its potential as a clean energy carrier, is poised to play a pivotal role in the global transition toward net-zero emissions (Kovač et al., 2021). With applications spanning transportation, industrial feedstocks, and electricity generation, hydrogen demand is expected to rise significantly in the coming decades (Qazi, 2022). In 2020, global hydrogen production was approximately 90 million metric tons (Mt) and is projected to increase steadily. According to the Hydrogen Council, achieving carbon neutrality by 2050 will necessitate an estimated 660 Mt of hydrogen, representing approximately 22% of the total global energy demand. However, a critical barrier to such large-scale hydrogen utilization is the availability of efficient and cost-effective storage solutions. Conventional surface storage technologies, such as cryogenic

tanks and high-pressure vessels, are limited by capacity constraints and high capital costs (Xie et al., 2024). Underground hydrogen storage (UHS) in porous media presents a viable alternative to overcome these storage challenges, facilitating the integration of hydrogen into the global energy landscape (Tarkowski, 2019; Zivar et al., 2021; Feng et al., 2024; Zhang et al., 2024).

Among various subsurface porous media, such as salt caverns and deep aquifers, depleted oil reservoirs offer significant advantages for underground hydrogen storage (UHS), including well-characterized geological structures, verified caprock integrity, and pre-existing infrastructure, all of which enhance their suitability for underground hydrogen storage (Sekar et al., 2023). For example, a field trial presented by Heller-schmid et al. (2024) reported an 84.3% hydrogen recovery for 119,353 m<sup>3</sup> of H<sub>2</sub> admixed with CH<sub>4</sub> in a depleted oil

reservoir after 285 days of storage. Kanaani et al. (2022) suggested that hydrogen recovery during UHS in a depleted oil reservoir could reach 89.7% if  $\text{CH}_4$  was used as the cushion gas according to their reservoir simulations. Lysyy et al. (2021) performed numerical simulations to investigate the storage of  $\text{H}_2$  with  $\text{CH}_4$  cushion gas in the mid-oil zone of the Norne field in Norway. The final hydrogen recovery in the oil zone reached 77% after 5 years. These high  $\text{H}_2$  recovery efficiencies highlight the strong potential of depleted oil reservoirs for hydrogen storage.

The rapid expansion of global shale gas and oil production over the past two decades has resulted in a large number of depleted shale reservoirs. These formations present attractive candidates for UHS.  $\text{H}_2$  recovery efficiency is largely determined by the flow dynamics and spatial distribution of  $\text{H}_2$  within the nanopores of the shale formation. These behaviors are affected by the interactions between the injected gases and the residual pore fluids, including water and oil. For example, Mashhadzadeh and Faroughi (2025) reported that confinement effects reduce  $\text{H}_2$  diffusion within slit nanopores, whereas higher temperatures weaken  $\text{H}_2$ -water interactions and consequently enhance its diffusivity. Wang et al. (2025) found that the presence of a water film along pore walls significantly suppresses  $\text{H}_2$  diffusion, but high pressures within the nanopores can disrupt such film and promote bypass flow. Zhang et al. (2023) investigated  $\text{H}_2$  dissolution in water-saturated kaolinite nanopores, revealing that nanoconfinement could enhance  $\text{H}_2$  solubility by up to 27 times in a 0.55 nm slit pore. Bechara et al. (2022) studied the impact of  $\text{H}_2$  on shale rocks and fluid properties to assess its potential for storage in depleted shale formations. Their results showed that  $\text{H}_2$  not only altered the wettability of shale but also affected the viscosity of both crude oil and produced water. A study by Chen et al. (2024) indicates that  $\text{CH}_4$  is preferentially adsorbed over  $\text{H}_2$  in a  $\text{CH}_4/\text{H}_2$  mixture, while  $\text{H}_2\text{O}$  molecules are preferentially adsorbed over both  $\text{CH}_4$  and  $\text{H}_2$  in a  $\text{CH}_4/\text{H}_2/\text{H}_2\text{O}$  mixture. Such preferential adsorption of  $\text{CH}_4$  and  $\text{H}_2\text{O}$  allows  $\text{H}_2$  molecules to move freely in the nanopores, facilitating their recovery during the  $\text{H}_2$  production process.

To date, researchers have mainly focused on  $\text{H}_2$  behaviors such as adsorption, diffusion, and dissolution in the presence of pore water; however, the influence of residual oil on these  $\text{H}_2$  properties remains poorly understood. Thus, this study, for the first time, investigates how the presence of crude oil affects  $\text{H}_2$  self-diffusion and spatial distribution within shale nanopores of varying sizes under a geological condition of 353 K and 30 MPa. The manuscript is organized as follows: Section 2 presents the methodology and details of the MD simulation. Section 3 begins with validation cases for the MD simulations, followed by an analysis and discussion of the behavior of the  $\text{H}_2$ -oil system in shale nanopores. Finally, Section 4 summarizes the conclusions and outlines future work.

## 2. Models and simulation details

In this study, molecular dynamics (MD) simulations were employed to investigate  $\text{H}_2$  behavior within nanopores in

the presence of residual oil. MD simulation is a powerful computational method grounded in statistical mechanics and thermodynamics. By applying Newton's laws of motion, MD tracks particle positions, velocities, and interaction forces over time, generating a trajectory that captures the system's molecular evolution. This trajectory enables detailed analysis of both static and dynamic properties, as well as the calculation of various macroscopic physical parameters. MD is especially valuable for conditions that are difficult or impossible to reproduce experimentally, such as extreme pressures and temperatures (Jin et al., 2021), nanoscale confinement (Liu et al., 2022, 2023, 2023a, 2024; Shi et al., 2025), interfacial phenomena (Chang et al., 2024, 2024a; Yang et al., 2017, 2025), and complex molecular interactions (Kollman and Merz Jr, 1990; Tuckerman and Martyna, 2000; Chang et al., 2023).

We used the Large-scale Atomic/Molecular Massively Parallel Simulator (LAMMPS) for all MD simulations (Thompson et al., 2022). Quartz ( $\alpha\text{-SiO}_2$ ) is one of the most common minerals in shale formations (Shaw and Weaver, 1965), thus it was used to build the shale nanopores. A unit cell of  $\alpha\text{-SiO}_2$  was obtained from the Materials Studio database and was cleaved along the [0, 0, 1] direction. Subsequently, it was replicated (supercell) in the x, y, and z directions to form a two-layer pore wall with dimensions of  $98.2 \text{ \AA} \times 49.1 \text{ \AA} \times 10.8 \text{ \AA}$ . By specifying a pore size (aperture) between the two pore walls, a slit nanopore model was developed. Four pore sizes including 2, 4, 6, and 8 nm were considered in this study. Moreover, to evaluate the impact of residual oil on gas behavior, varying amounts of crude oil (expressed as oil saturation,  $S_o$ ) were introduced into the nanopores along with  $\text{H}_2$ . Different oil components, including n-methane ( $\text{C}_1$ ), n-butane ( $\text{C}_4$ ), n-octane ( $\text{C}_8$ ), and n-dodecane ( $\text{C}_{12}$ ), were separately incorporated as representative crude oil components to study how different hydrocarbons influence  $\text{H}_2$  behaviors within the nanopores.

In the simulations,  $\text{H}_2$  and oil molecules were randomly placed in the nanopore space at the initial condition. A 10 ns NVT run with a 1 fs time step was then performed to allow each system to reach equilibrium, with the temperature controlled using a Nosé-Hoover thermostat. During all simulations, the quartz surfaces were kept fixed, remaining stationary and rigid. The classical TraPPE force field with a united-atom (UA) style was used to model the interactions of the oil molecules.  $\text{H}_2$  molecules were modelled using a validated single-site force field (Köster et al., 2018), while the  $\text{SiO}_2$  layers were described using force fields developed by Cui et al. (2021) and Yu et al. (2023). These force fields have been validated for their reliability in simulating the related materials (Mosher et al., 2013; Xiong et al., 2017; Van Rooijen et al., 2023; Chang et al., 2023, 2026). The self-diffusion coefficient of the  $\text{H}_2$  was calculated using the mean square displacement (MSD). MSD quantifies the average squared deviation of a particle's position from its initial location over time and is defined as (Yang et al., 2020):

$$MSD(t) = \left\langle |r_i(t) - r_i(0)|^2 \right\rangle \quad (1)$$

where  $r_i(t)$  is the position of particle  $i$  at time  $t$ , and the angular

brackets denote an ensemble average. The self-diffusion coefficient ( $D$ ) in a three-dimensional scale can then be obtained from the MSD via:

$$D = \lim_{t \rightarrow \infty} \frac{1}{6t} MSD(t) \quad (2)$$

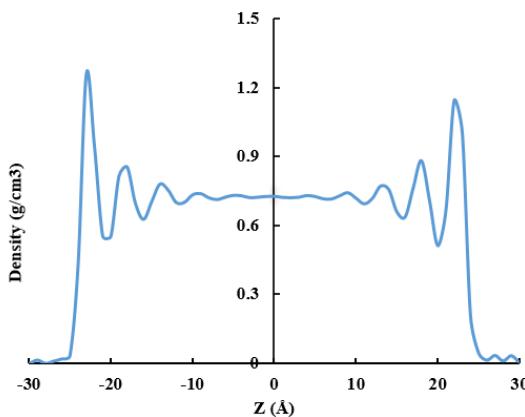
### 3. Results and discussions

Validation of the molecular model and force field parameters is crucial for reliable MD simulation analysis. Density is an important property for validating force fields. Therefore, densities of  $H_2$ ,  $C_1$ , and  $C_8$  (representing long-chain n-alkanes) at 353 K and 30 MPa were determined and compared with values from the NIST database. As listed in Table 1, densities determined from our MD simulations agree well with the reference data.

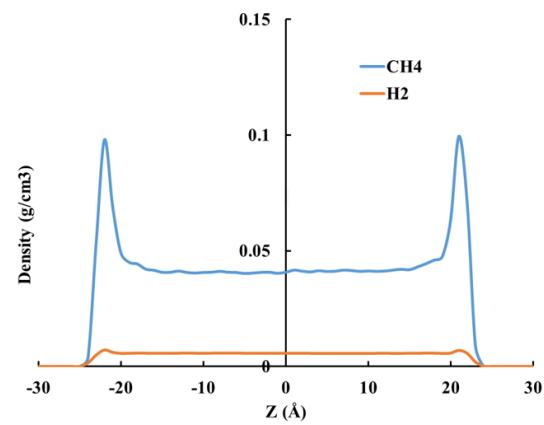
**Table 1.** Density validation between MD simulation results and reference data.

	MD	NIST (g/cm <sup>3</sup> )
$H_2$	0.0177	0.0177
$C_1$	0.163	0.167
$C_8$	0.684	0.686

In addition, we determined the density distribution profile of pure  $C_8$  in a 5 nm quartz nanopore at 353 K and 30 MPa, as shown in Fig. 1. The obtained profile is consistent with the results reported by Wang et al. (2016), validating the force field used to simulate the interaction between the quartz nanopore and long-chain n-alkanes. Moreover, we specially constructed an  $H_2/C_1$  mixture system (1:1 mole ratio) in a 5 nm quartz nanopore at approximately 343 K and 15 MPa, and determined the  $H_2/C_1$  density profiles separately, as shown in Fig. 2. The density profiles of  $H_2$  and  $C_1$  are in good agreement with the results reported by Chen et al. (2024) under similar pressure and temperature conditions, further validating the force fields used to simulate the interactions between  $H_2$ ,  $C_1$  and the shale nanopore.

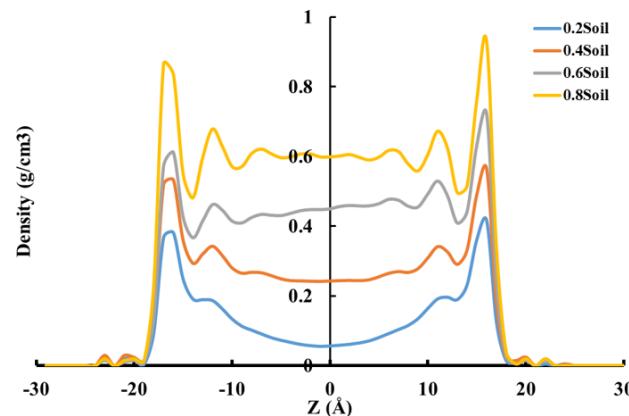


**Fig. 1.** Density profile of  $C_8$  in the 5 nm slit pore at 353 K and 30 MPa.



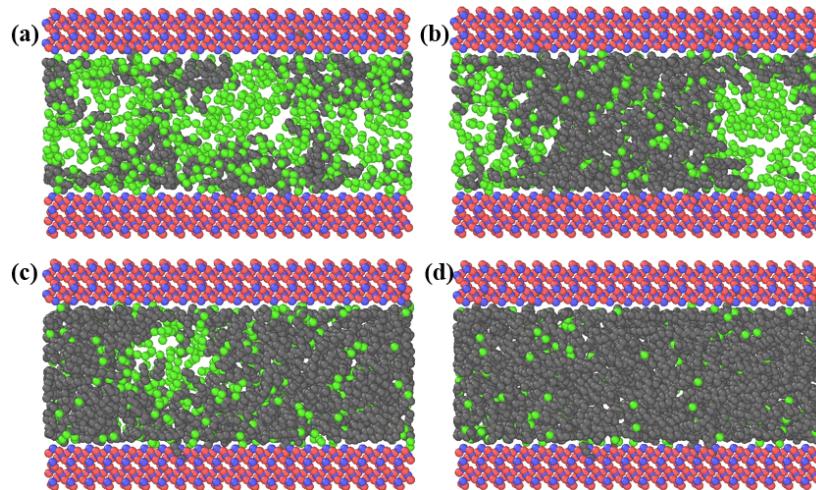
**Fig. 2.** Density profiles of  $C_8/C_1$  gas mixture in a 5 nm slit pore at 343 K and 15 MPa.

To study the behavior of the  $H_2$ -oil system in nanopores, we first visualize the configuration of the  $H_2$ - $C_8$  system in a 4 nm slit pore with different oil saturations as an example, as shown in Fig. 3. In addition, the corresponding density profiles of  $C_8$  and  $H_2$  across the nanopore were determined and presented in Figs. 4 and 5. At a low oil saturation of 0.2, Fig. 3 shows that oil molecules tend to aggregate into clusters and accumulate on the pore surface, while  $H_2$  molecules mainly reside in the center of the pore space, which is consistent with their density distribution profiles. As oil saturation increases, the oil phase expands and reduces the space available for  $H_2$  molecules to move. At an oil saturation of 0.6, a small amount of  $H_2$  molecules forms a gas bubble. At the highest oil saturation of 0.8, the gas phase no longer exists. Instead,  $H_2$  molecules dissolve into the oil phase, and some accumulate on the pore surface. Unlike residual pore water, which can effectively inhibit  $H_2$  accumulation on the quartz surface (Chen et al., 2024),  $H_2$  accumulation on the quartz surface is observed at all oil saturation levels, although it is weakened by the presence of oil. This behavior may lead to  $H_2$  loss during hydrogen storage in depleted shale reservoirs.



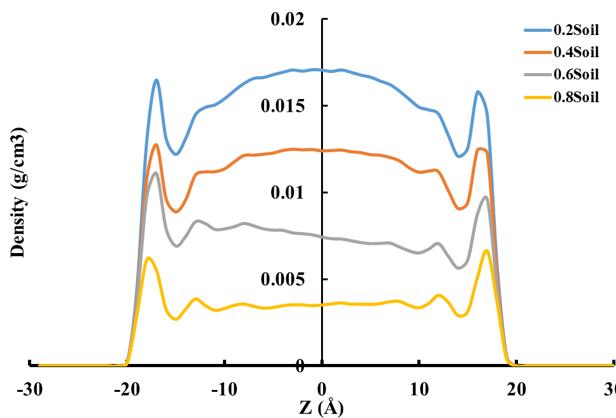
**Fig. 4.** Density profiles of  $C_8$  in the  $H_2$ - $C_8$  system within a 4 nm nano pore at different oil saturations.

To investigate the impact of pore aperture on the behavior of  $H_2$  and oil in quartz nanopores, the configuration of the  $H_2$ - $C_8$  system with 0.2 oil saturation in nanopores with different



**Fig. 3.** Configurations of the  $\text{H}_2$ - $\text{C}_8$  system in a 4 nm slit pore with different oil saturations, (a) 0.2 Soil, (b) 0.4 Soil, (c) 0.6 Soil, and (d) 0.8 Soil. Black:  $\text{C}_8$  molecules, green:  $\text{H}_2$ .

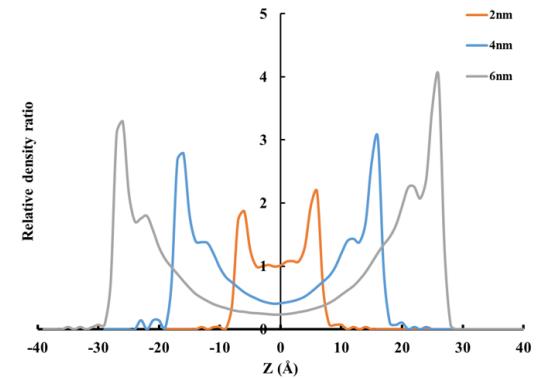
apertures is visualized in Fig. 6 as a representative example. In addition, the relative density ratio, defined as the local density in the nanopores divided by the bulk density, was determined in Figs. 7 and 8 to illustrate the preferential distribution of  $\text{H}_2$  and oil in nanopores with different apertures. According to the configurations and density profiles, it is clear that oil molecules mainly distribute near the pore surface. However, as the pore aperture decreases, the oil relative density ratio in the middle region increases, indicating that oil molecules move more easily into the central region of the nanopore with smaller apertures. In addition, the relative density ratio of  $\text{H}_2$  near the pore surface increases as the pore aperture decreases, indicating that the nano-confinement effect enhances the accumulation of  $\text{H}_2$  on the pore surface even in the presence of residual oil.



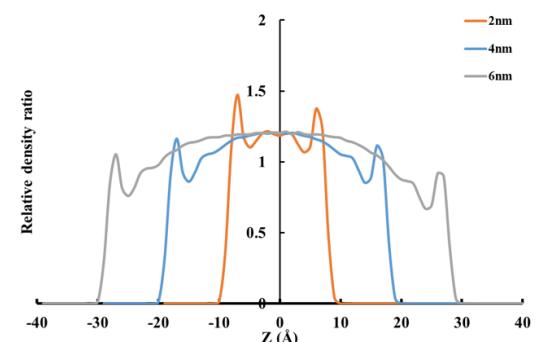
**Fig. 5.** Density profiles of  $\text{H}_2$  in the  $\text{H}_2$ - $\text{C}_8$  system within a 4 nm nano pore at different oil saturations.

The self-diffusion coefficients of  $\text{H}_2$  in the  $\text{H}_2$ - $\text{C}_8$  system with varying oil saturations in nanopores with different apertures are shown in Fig. 9. As oil saturation increases, more oil molecules occupy the pore space, constricting the movement of  $\text{H}_2$  molecules and leading to a consistent decrease in  $\text{H}_2$  self-diffusion. Moreover, as the pore aperture decreases, we

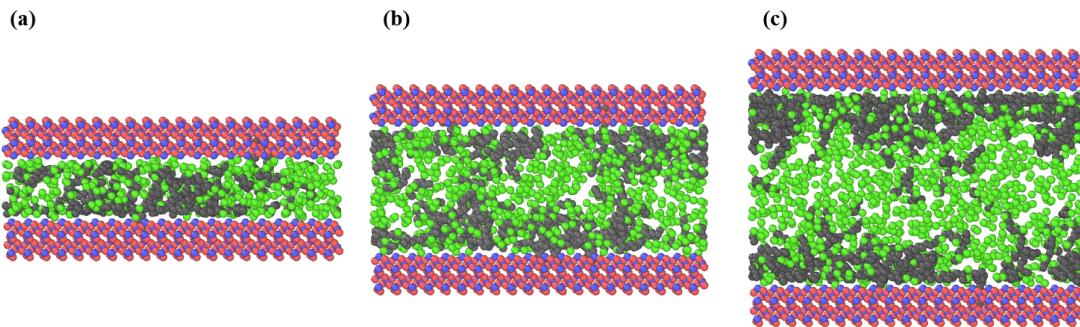
believe there are two reasons that contribute to the decrease in  $\text{H}_2$  self-diffusion coefficients. First, the nano-confinement effect is enhanced as the aperture decreases, slowing down gas self-diffusion (Spera and Franco, 2020; Lyu et al., 2022). Second, in smaller nanopores, oil molecules can more easily move toward the center of the pore compared to larger nanopores, which may also restrict  $\text{H}_2$  self-diffusion within the nanopores.



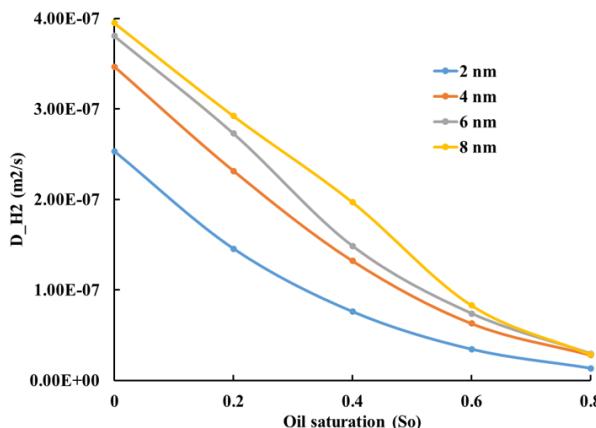
**Fig. 7.** Relative density ratio of  $\text{C}_8$  in the  $\text{H}_2$ - $\text{C}_8$  system with 0.2 oil saturation in nanopores with different sizes.



**Fig. 8.** Relative density ratio of  $\text{H}_2$  in the  $\text{H}_2$ - $\text{C}_8$  system with 0.2 oil saturation in nanopores with different sizes.



**Fig. 6.** Configurations of  $\text{H}_2$ - $\text{C}_8$  system with 0.2 oil saturation in nanopores with (a) 2 nm aperture, (b) 4 nm aperture, and (c) 6 nm aperture.

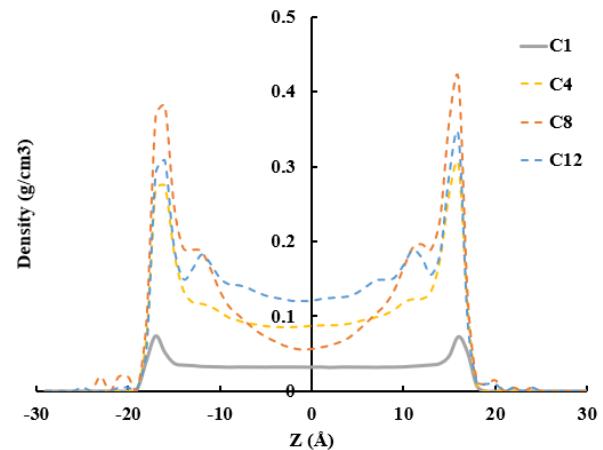


**Fig. 9.** Self-diffusion coefficients of  $\text{H}_2$  in the  $\text{H}_2$ - $\text{C}_8$  system within nanopores with different pore sizes.

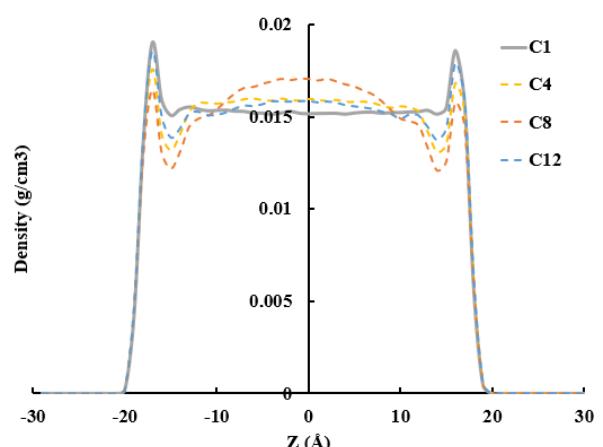
In addition to  $\text{C}_8$ , the behavior of  $\text{H}_2$  in interactions with other common oil components within quartz nanopores was also investigated, including  $\text{C}_1$ ,  $\text{C}_4$ , and  $\text{C}_{12}$ . As an example, at an oil saturation of 0.2, the configurations of  $\text{H}_2$  with  $\text{C}_1$ - $\text{C}_{12}$  separately in a 4 nm nanopore are shown in Fig. 10, and the corresponding density profiles of oil and  $\text{H}_2$  are depicted in Figs. 11 and 12 respectively. At 353 K and 30 MPa,  $\text{C}_1$  exists in a supercritical state, whereas  $\text{C}_4$ ,  $\text{C}_8$ , and  $\text{C}_{12}$  are in the liquid phase. Consequently, as shown in Fig. 10(a),  $\text{C}_1$  readily mixes with  $\text{H}_2$ , and the densities of  $\text{H}_2$  and  $\text{C}_1$  are relatively uniformly distributed along the nanopore, with pronounced accumulation near the pore surface. In contrast, the liquid components  $\text{C}_4$ ,  $\text{C}_8$ , and  $\text{C}_{12}$  mix less readily with gaseous  $\text{H}_2$ , leading to the formation of oil clusters (Figs. 10(b) and 10(c)) and oil-bridging (Fig. 10(d)) structures within the nanopore. Correspondingly, oil clusters of  $\text{C}_4$  and  $\text{C}_8$  on the pore surface result in high oil densities near the pore wall, whereas the formation of an oil bridge by  $\text{C}_{12}$  leads to higher oil densities in the central region of the nanopore compared to the clustered cases.

Fig. 13 shows the  $\text{H}_2$  self-diffusion coefficients within a 4 nm nanopore in the presence of different oils. For the  $\text{H}_2$ - $\text{C}_1$  system, since  $\text{C}_1$  has a larger molecular weight than  $\text{H}_2$  and diffuses more slowly than  $\text{H}_2$ , its interaction with  $\text{H}_2$  leads to a reduction in the self-diffusion coefficient of  $\text{H}_2$ . In addition, as the amount of  $\text{C}_1$  present in the nanopore increases, the

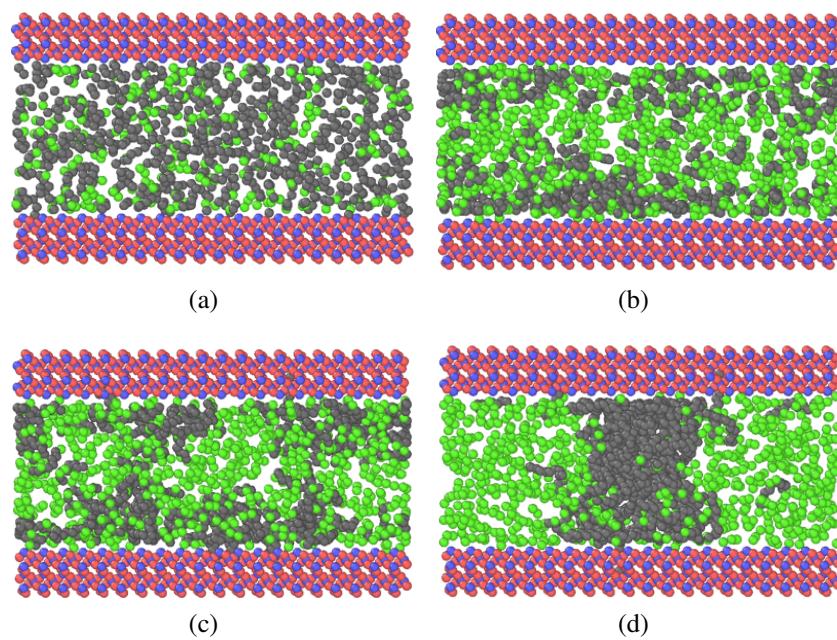
interaction between  $\text{H}_2$  and  $\text{C}_1$  is further enhanced, resulting in an additional decrease in  $\text{H}_2$  self-diffusion. A significant reduction in  $\text{H}_2$  self-diffusion is observed when  $\text{H}_2$  coexists with  $\text{C}_4$ ,  $\text{C}_8$ , and  $\text{C}_{12}$ . This is likely because these oil components with larger MW are in the liquid state under simulated conditions and do not mix with  $\text{H}_2$  as readily as  $\text{C}_1$ , occupying the pore volume and restricting the space available for  $\text{H}_2$  transport, thereby markedly reducing  $\text{H}_2$  self-diffusion.



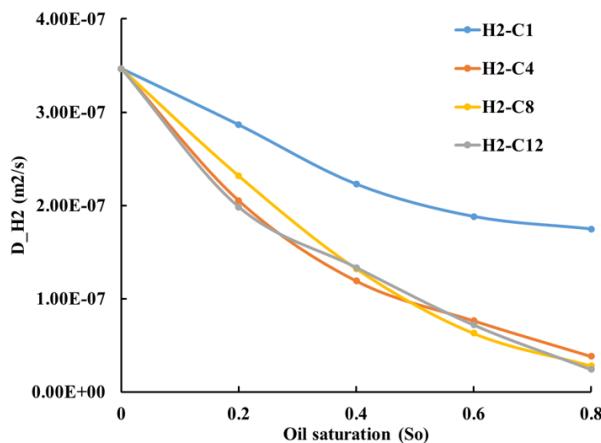
**Fig. 11.** Oil density profiles in a 4 nm nanopore at 0.2 oil saturation for  $\text{C}_1$ - $\text{C}_{12}$  separately.



**Fig. 12.**  $\text{H}_2$  density profiles in a 4 nm nanopore at 0.2 oil saturation with  $\text{C}_1$ - $\text{C}_{12}$  separately.



**Fig. 10.** Configurations of the H<sub>2</sub>-oil system at an oil saturation of 0.2 in a 4 nm nanopore for (a) C<sub>1</sub>, (b) C<sub>4</sub>, (c) C<sub>8</sub> and (d) C<sub>12</sub>.



**Fig. 13.** Self-diffusion coefficients of H<sub>2</sub> in a 4 nm nanopore with different n-alkanes.

#### 4. Conclusions and outlook

In this study, molecular dynamics simulations were employed to systematically investigate the behavior of H<sub>2</sub> in shale nanopores in the presence of residual oil, with particular emphasis on the effects of oil saturation, pore aperture, and oil composition. The results demonstrate that residual oil cannot completely inhibit H<sub>2</sub> accumulation on the pore surface. H<sub>2</sub> accumulation is observed at all oil saturation levels, although it is weakened by the presence of oil, suggesting a potential mechanism for H<sub>2</sub> loss during underground hydrogen storage (UHS) in depleted shale reservoirs. Oil molecules preferentially adsorb near the pore surface, while decreasing pore aperture promotes oil migration toward the central region of the nanopore. Simultaneously, as pore size decreases, the

nano-confinement effect enhances H<sub>2</sub> surface accumulation even in the presence of residual oil. These confinement effects, together with increasing oil saturation, significantly reduce H<sub>2</sub> self-diffusion by constricting its transport pathway. Furthermore, the impact of oil composition on H<sub>2</sub> behavior is found to be strongly phase dependent. Supercritical C<sub>1</sub> readily mixes with H<sub>2</sub>, resulting in relatively uniform density distributions, whereas liquid C<sub>4</sub>, C<sub>8</sub>, and C<sub>12</sub> exhibit poor miscibility with H<sub>2</sub> and form oil clusters or oil-bridging structures that significantly restrict H<sub>2</sub> mobility. Based on this study, future work should focus on experimental validation of these simulation results and extend to the investigation of key factors relevant to UHS. In particular, the effects of cushion gases (e.g., CO<sub>2</sub> and N<sub>2</sub>) and geological conditions, such as pressure, temperature, and salinity, on H<sub>2</sub>-oil behavior and n-alkane phase states should be systematically examined. Such studies will further strengthen understanding and provide a solid basis for the design of efficient underground hydrogen storage strategies in depleted shale reservoirs.

#### Conflict of interest

The authors declare no competing interest.

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